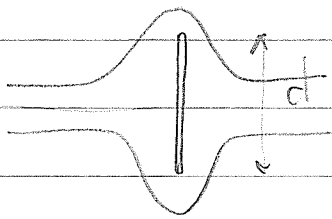


- { Displacement thickness from XI }
- { Skin friction from XI }
- { Momentum loss thickness from XI }

Pressure drag & friction drag { Show Eq. 2.21 }

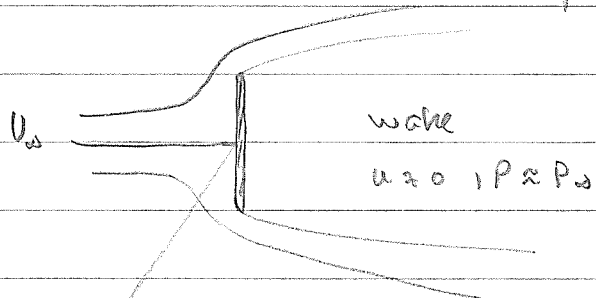
Blunt body

irrotational flow



drag $D'_i = 0$

real flow $Re \gg 1$

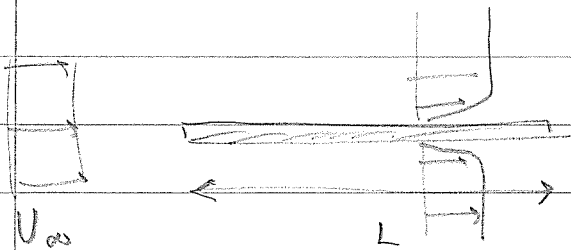


$$p_0 = p_\infty + \frac{1}{2} \rho U_\infty^2$$

Form drag $D'_f = \frac{1}{2} \rho U_\infty^2 C_d \cdot d$

drag coefficient ~ 1 for blunted body { show alt C_d }

Streamlined body



Friction drag

$$D'_f = \rho U_\infty^2 L \cdot 0.664 \sqrt{\frac{\nu L}{U_\infty}}$$

$$= \rho U_\infty^2 L \cdot 1.4 = \rho U_\infty^2 \frac{2.8 L}{\sqrt{Re_L}}$$

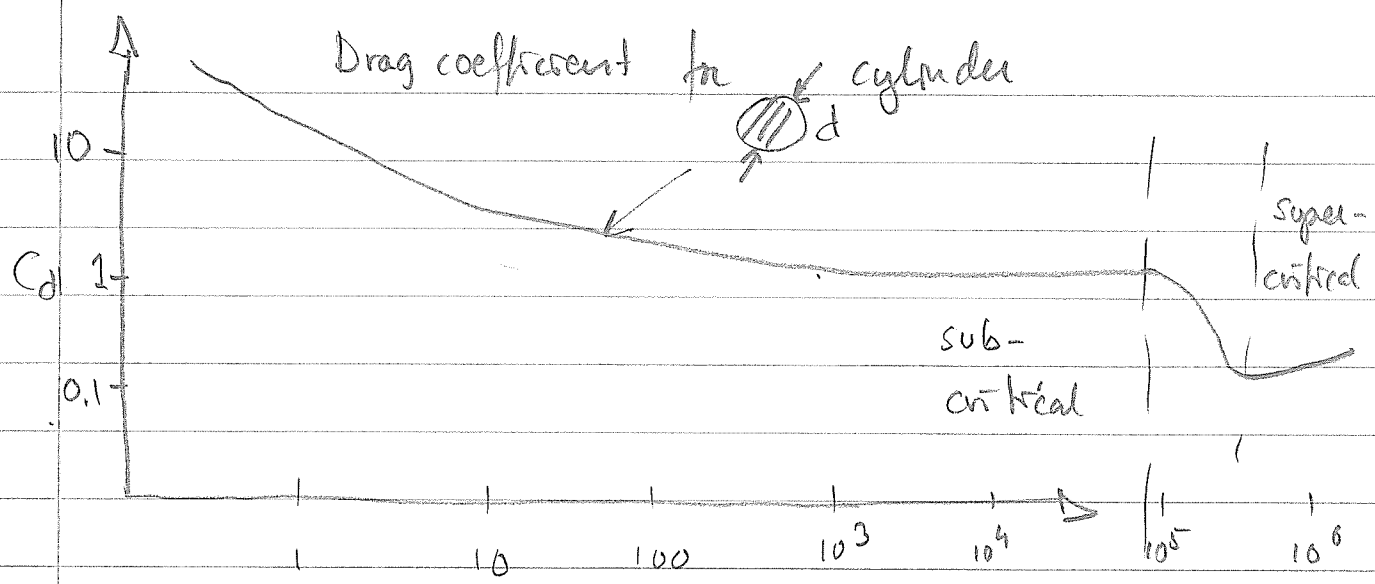
$$= \rho U_\infty^2 \frac{2.8 L}{C_d}$$

Plate length for equal drag $\frac{1}{2} \rho U_\infty^2 \cdot d = \frac{1}{2} \rho U_\infty^2 \cdot \frac{2.8 L}{\sqrt{Re_L}}$

$$\frac{L}{d} = \frac{\sqrt{Re_L}}{2.8}$$

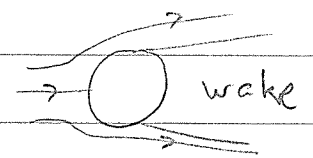
$$Re_L \sim 10^6 \Rightarrow \frac{L}{d} = \frac{1000}{2.8} = \underline{\underline{357}} \sqrt{Re_L}$$

$$Re_d \sim 10^6 / 357 \sim 3 \cdot 10^3$$

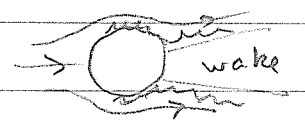


$$Re = \frac{U_{\infty} d}{\nu}$$

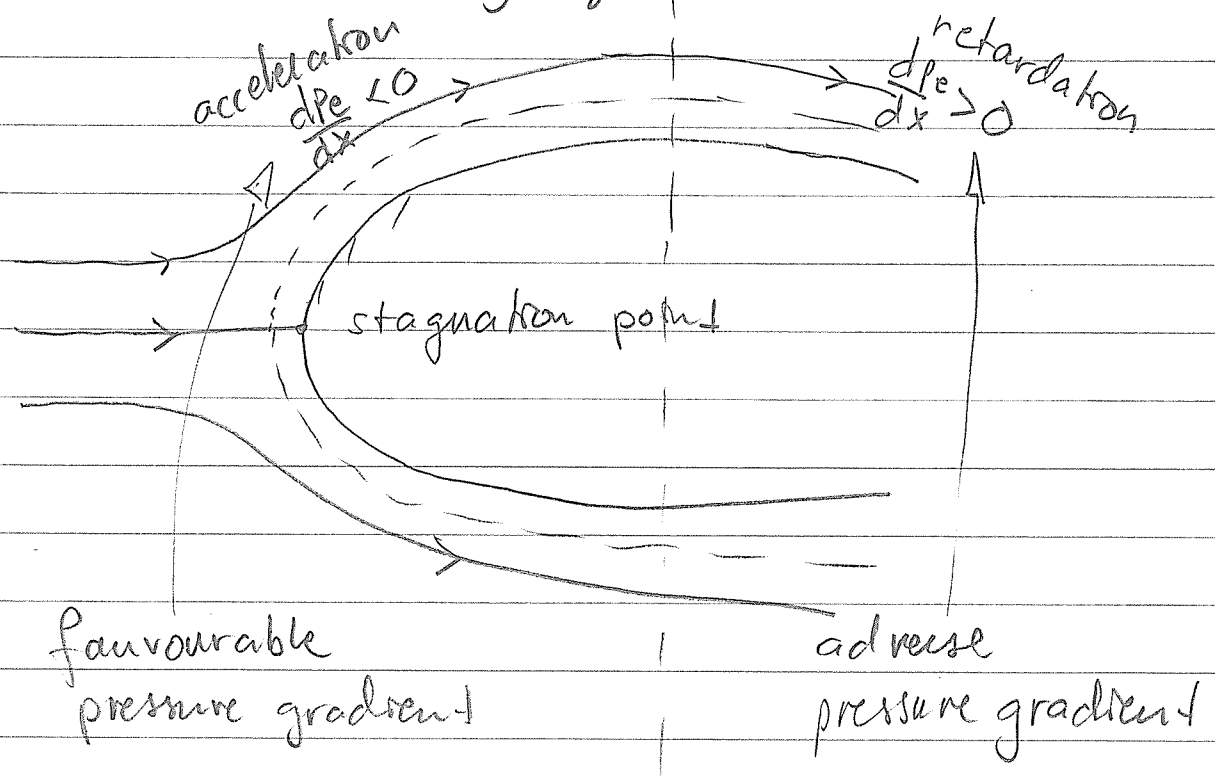
subcritical regime - laminar b.l.



supercritical regime - turbulent b.l.



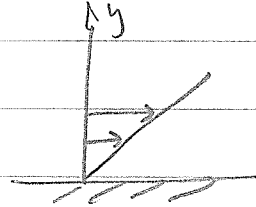
Separation of boundary layer from solid surface - connected to pressure gradient, $\frac{dp_e}{dx} > 0$, in the boundary layer



Effect on boundary layer profile.

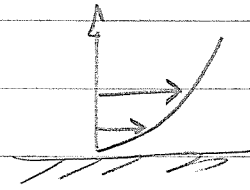
at the wall $0 = -\frac{1}{\rho} \frac{d p_e}{d x} + \nu \frac{\partial^2 u}{\partial y^2} \Big|_{y=0}$

$\frac{d p_e}{d x} = 0 \Rightarrow \frac{\partial^2 u}{\partial y^2} \Big|_{y=0} = 0$



$\frac{d p_e}{d x} < 0 \Rightarrow \frac{\partial^2 u}{\partial y^2} \Big|_{y=0} < 0$

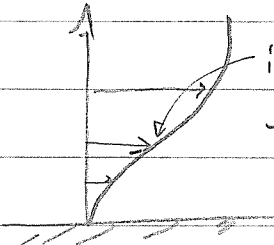
accelerating



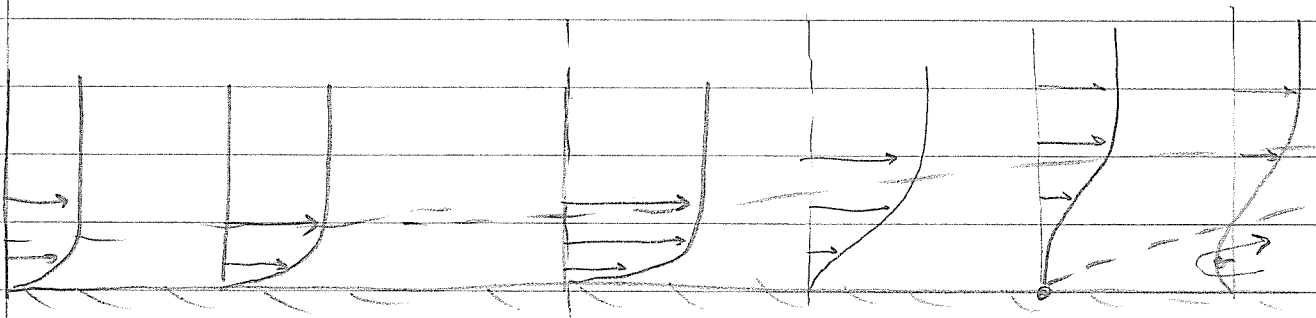
fuller profile,
thinner b.l.

$\frac{d p_e}{d x} > 0 \Rightarrow \frac{\partial^2 u}{\partial y^2} \Big|_{y=0} > 0$

decelerating



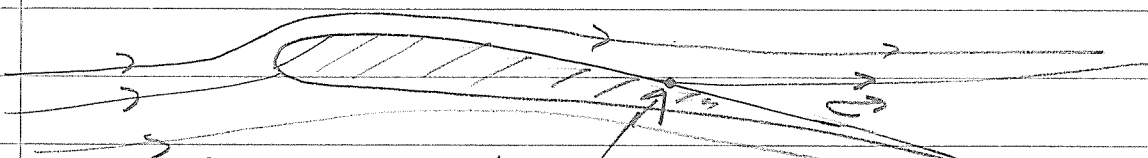
inflection point,
thicker b.l.



$\frac{d p_e}{d x} < 0$

$\frac{d p_e}{d x} > 0$

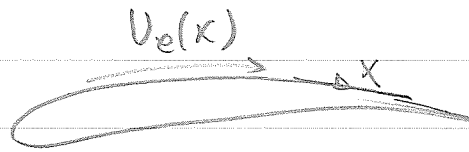
At separation point $\frac{\partial u}{\partial y} \Big|_{y=0} = 0$



tangential separating streamline

Boundary layer theory not valid beyond separation point.

Falkner-Skan similarity solutions



For which inviscid flows $U_e(x)$ exist self-similar boundary layers?

$$u(x,y) = U_e(x) f'(\eta) \quad ; \quad \eta = y/\delta(x)$$

$$\psi = \int^y U_e(x) f'(\eta) dy = U_e(x) \delta(x) f(\eta)$$

$$v(x,y) = -\left(\frac{\partial \psi}{\partial x}\right)_y = -\left(U_e \delta\right)' f - U_e \delta f' \left(-\eta \frac{\delta'}{\delta}\right)$$

⇒

$$f''' + \frac{1}{2}(\beta+1) f f'' + \beta(1-f'^2) = 0$$

$$\delta(x) = \sqrt{\frac{\nu x}{U_e(x)}} \quad ; \quad \beta = \frac{x}{U_e} \frac{dU_e}{dx}$$

Possible inviscid flows $U_e(x) = U_L \left(\frac{x}{L}\right)^\beta$
for similarity solution

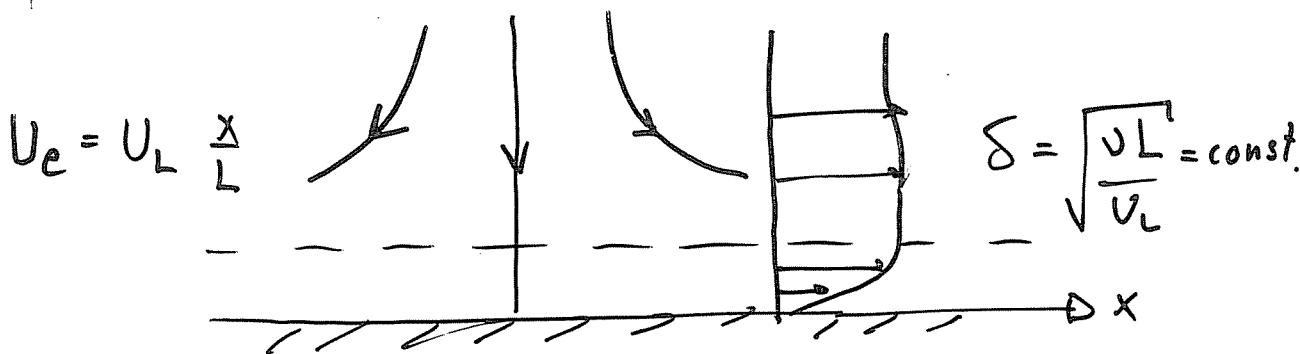
$$f(0) = f'(0) = 0, \quad f'(\infty) = 1$$

Falkner-Skan flows

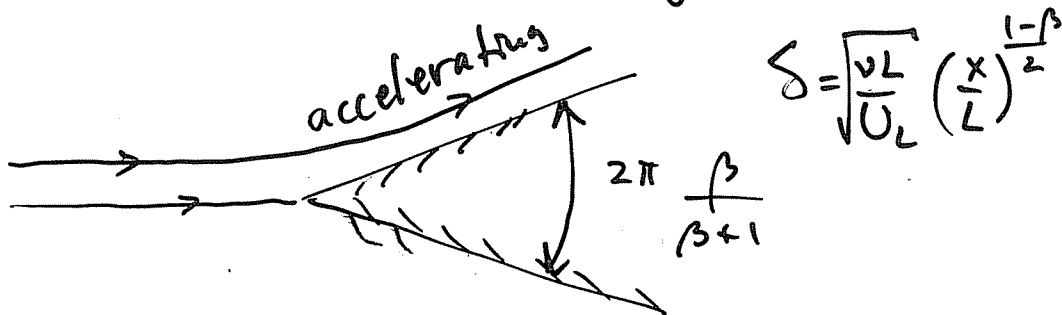
$\beta = 0$ Blasius flat plate



$\beta = 1$ Stagnation point flow



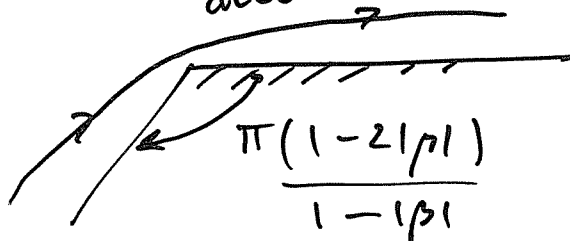
$0 < \beta < 1$: Flow towards wedge



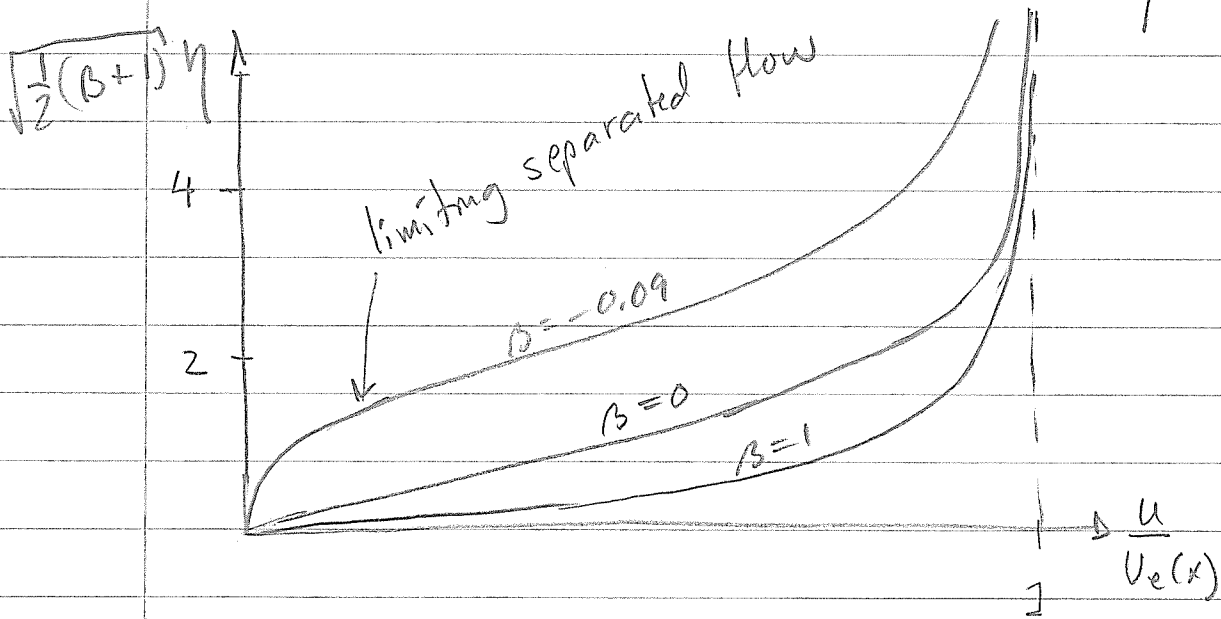
$\beta < 0$

Flow around corner
decelerating flow

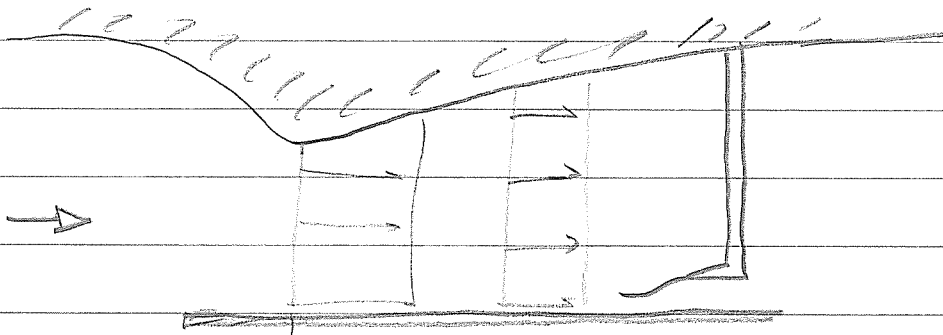
$$\delta = \sqrt{\frac{\nu L}{U_L}} \left(\frac{x}{L}\right)^{\frac{1+|\beta|}{2}}$$



Numerical solution exist for $-0.0904 < \beta$



Experimental investigation of laminar boundary layers with and without pressure gradients.



decelerating flow along plate, $\frac{dp_e}{dx} > 0$

Measure: * pressure distribution along plate

* boundary layer velocity profiles, 2 stations

Comparison with "equivalent" Falkner-Skan solution.