

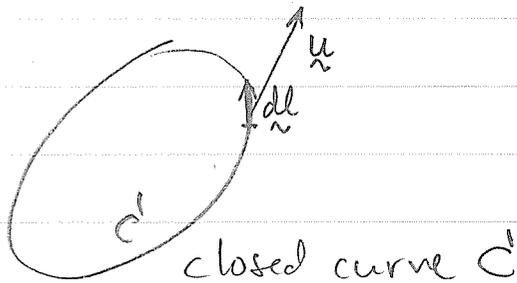
Vorticity dynamics.

Basic vortex flows

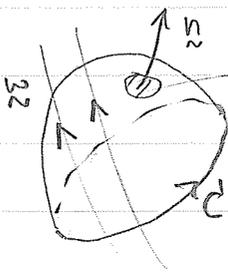
$u_\varphi = \frac{1}{2} \omega r$ solid body rotation
 vorticity $\omega_z = \omega$
 (homogeneous distribution of vorticity)

$u_\varphi = \frac{\Gamma}{2\pi r}$ irrotational vortex / line vortex
 vorticity $\omega_z = 0$
 (infinite vorticity at origin)

Definition: Circulation $\Gamma = \oint_C \vec{u} \cdot d\vec{l}$



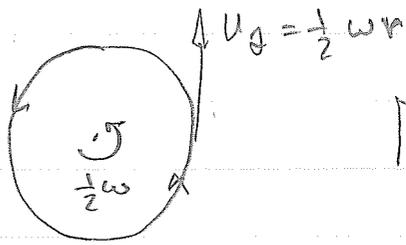
Stoke's theorem: $\oint_C \vec{u} \cdot d\vec{l} = \iint_M \nabla \times \vec{u} \cdot \vec{n} \, dS = \iint_M \vec{\omega} \cdot \vec{n} \, dS$



$|\vec{\omega}|$ is circulation/unit area

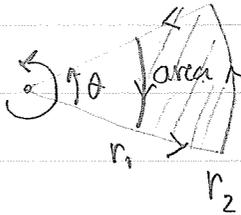
$= \iint_M |\vec{\omega}| \underbrace{n_w}_{\text{projected } dS \perp \text{ to } \vec{\omega}} \, dS$

Solid b.r.



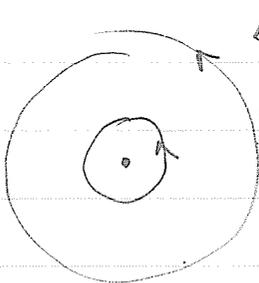
$$\Gamma = \oint u_{\theta} r d\theta = \frac{1}{2} \omega r^2 2\pi$$

$$= \omega \underbrace{\pi r^2}_{\text{area}}$$



$$\Gamma_{\theta} = \frac{1}{2} \omega r_2^2 \theta - \frac{1}{2} \omega r_1^2 \theta = \omega \underbrace{\frac{\theta}{2} (r_2^2 - r_1^2)}_{\text{area}}$$

Line vortex

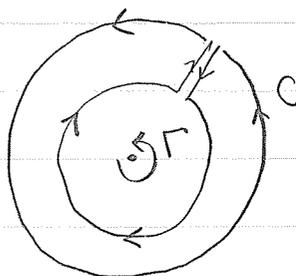


$$u_{\theta} = \frac{\Gamma}{2\pi r} \quad \Gamma = \oint \frac{\Gamma}{2\pi r} r d\theta = \Gamma$$

Γ is the strength of line vortex.

Although $\omega_z = 0$, $\Gamma \neq 0$ for all C enclosing the vortex.

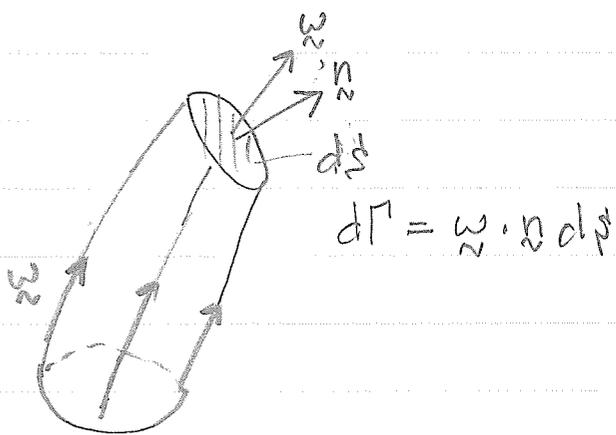
Curve not enclosing (ex.)



$$\Gamma_C = \frac{\Gamma}{2\pi r_2} \cdot r_2 2\pi - \frac{\Gamma}{2\pi r_1} \cdot r_1 2\pi = 0$$

All vorticity concentrated to vortex centre.

Vortex lines



vortex tube

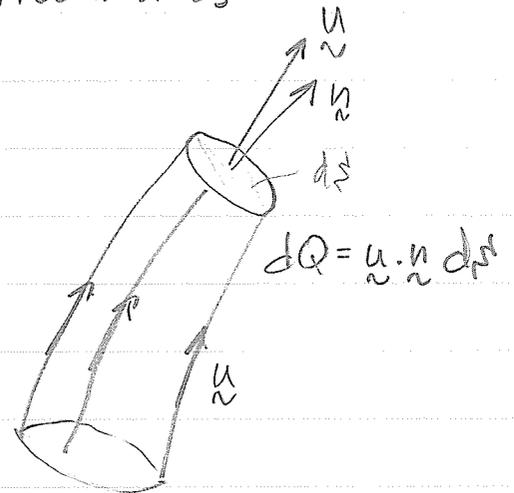
$$\vec{\omega} = \nabla \times \vec{u}$$

$$\Rightarrow \nabla \cdot \vec{\omega} = 0$$

analogous to $\nabla \cdot \vec{u} = 0$

for incompressible flow

streamlines



stream tube

Viscous stress $\tau_{ij} = 2\mu \bar{e}_{ij} + \mu_B \bar{e}_{ij}$

solid body rotation $\bar{e}_{ij} = \bar{e}_{ij} = 0$ no deformation
 \Rightarrow no viscous stress

irrotational flow deformation rate $\neq 0 \Rightarrow \tau_{ij} \neq 0$

Viscous force/unit volume $\frac{\partial (\tau_{ij})}{\partial x_j} = -\mu (\nabla \times \vec{\omega})_i$

$= 0$ for $\vec{\omega} = \text{const.}$ and for irrotational flow.

Kelvin's circulation theorem.

If: a) inviscid flow $\nu_{ij} = 0$ or $Re \rightarrow \infty$

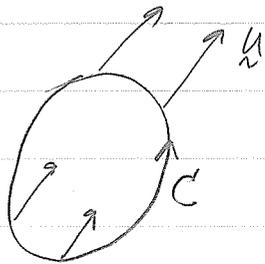
b) conservative body force $\underline{f} = -\nabla \Pi$

e.g. $\Pi = -\underline{g} \cdot \underline{x}$

c) barotropic flow $\rho(p)$

e.g. $\rho = \text{const.}$ or isentropic flow $p/\rho^\gamma = \text{const.}$

then:



material curve C

$$\Gamma = \oint_{C(t)} \underline{u} \cdot d\underline{x}$$

$$\boxed{\frac{D}{Dt} \Gamma = 0}$$

Proof:

$$\frac{D}{Dt} \Gamma = \frac{D}{Dt} \oint u_i dx_i = \underbrace{\oint \frac{Du_i}{Dt} dx_i}_I + \underbrace{\oint u_i \frac{D}{Dt} dx_i}_{II}$$

$$II = \oint_C u_i du_i = \oint_C d\left(\frac{u_i u_i}{2}\right) = 0$$

$$I = \oint_C \left(-\frac{1}{\rho} \frac{\partial p}{\partial x_i} + f_i + \frac{1}{\rho} \frac{\partial}{\partial x_j} (\tau_{ij}) \right) dx_i$$

$= 0$ for $\mu = 0$

$$\oint_C \frac{1}{\rho} dp = \oint_C \frac{dF(\rho)}{d\rho} d\rho = \oint_C dF = 0$$

$$\oint -\frac{\partial \pi}{\partial x_i} dx_i = -\oint d\pi = 0$$

$$\Rightarrow \frac{D\pi}{Dt} = 0 \quad \cancel{\neq}$$

Irrrotational flow at $t=0$ $\underline{\omega}(t=0) = 0$
(except at singular points of line vortex)

$$\Gamma(t=0) = \iint_S \underline{\omega} \cdot \underline{n} dS = 0 \quad \text{for any curve}$$

C (not enclosing the line vortex) and surface S .

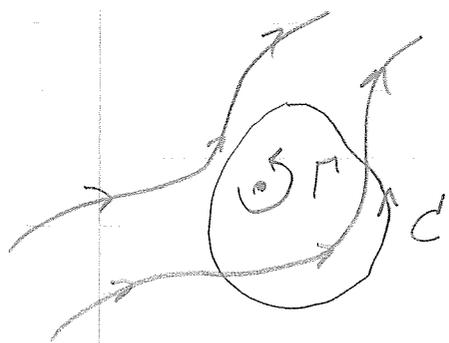
then since $\frac{D\Gamma}{Dt} = 0$ for any curve

$$\Rightarrow \Gamma = \iint_S \underline{\omega}(t) \cdot \underline{n} dS = 0 \quad \text{for any surface } S$$

thus $\underline{\omega}(t) = 0$.

Irrrotational flow remains irrotational
under the conditions of Kelvin's theorem.

Irrotational flow with line vortex Γ .



$$\frac{D}{Dt} \Gamma_c = 0, \quad \Gamma_c = \Gamma = \text{constant}$$

the material curve will enclose the vortex at all times

Material curves not enclosing the vortex

$$\frac{D}{Dt} \Gamma_c = 0, \quad \Gamma_c = 0$$

Helmholtz theorems (same conditions as Kelvin's)

- vortex lines are material lines and move with the fluid
- the strength of a line vortex, i.e. Γ , remains constant in time
- the strength of a line vortex is constant along its length
- a line vortex cannot end within the fluid (closed loops or end at solid wall)

Derivation of the vorticity equation.

$$\left\{ \begin{array}{l} \frac{\partial \underline{u}}{\partial t} + \underline{u} \cdot \nabla \underline{u} = -\frac{1}{\rho} \nabla p + \underline{f} + \nu \nabla^2 \underline{u} \\ \nabla \cdot \underline{u} = 0 \end{array} \right. \quad \text{allow for small variations of } \rho$$

$$\underline{\omega} = \nabla \times \underline{u} \quad \text{vorticity vector}$$

$$\omega_i = \epsilon_{ijk} \frac{\partial u_k}{\partial x_j}$$

$$\begin{aligned} \text{use: } \underline{u} \cdot \nabla \underline{u} &= \frac{1}{2} \nabla (\underline{u} \cdot \underline{u}) - \underline{u} \times (\nabla \times \underline{u}) \\ &= \frac{1}{2} \nabla (\underline{u} \cdot \underline{u}) + \underline{\omega} \times \underline{u} \end{aligned}$$

$$[\text{since: } \underline{a} \times (\underline{b} \times \underline{c}) = \underline{b} \underline{a} \cdot \underline{c} - \underline{c} \underline{a} \cdot \underline{b} \text{ then}]$$

$$\underline{u} \times (\nabla \times \underline{u}) = \nabla \left(\frac{\underline{u} \cdot \underline{u}}{2} \right) - \underline{u} \cdot \nabla \underline{u}$$

$$\nabla \times \left[\frac{\partial \underline{u}}{\partial t} + \frac{1}{2} \nabla (\underline{u} \cdot \underline{u}) + \underline{\omega} \times \underline{u} = -\frac{1}{\rho} \nabla p + \underline{f} + \nu \nabla^2 \underline{u} \right]$$

$$\text{note } \nabla \times \nabla(\cdot) = 0$$

$$\nabla \times (\underline{\omega} \times \underline{u}) = \nabla \times (\underline{\omega} \times \underline{u}) + \nabla \times (\underline{\omega} \times \underline{u}) =$$

$$= \underline{u} \cdot \nabla \underline{\omega} - \underline{u} \underbrace{\nabla \cdot \underline{\omega}}_{=0} + \underline{\omega} \underbrace{\nabla \cdot \underline{u}}_{=0} - \underline{\omega} \cdot \nabla \underline{u}$$

$$\frac{\partial \omega_k}{\partial x_i} = \epsilon_{ijk} \frac{\partial u_l}{\partial x_j} \frac{\partial u_l}{\partial x_i} = \epsilon_{ijk} \frac{\partial^2 u_l}{\partial x_k \partial x_i} = 0$$

[good exercise is to derive this with tensor notation] VII.8

$$\frac{\partial \underline{\omega}}{\partial t} + \underline{u} \cdot \nabla \underline{\omega} = \underline{\omega} \cdot \nabla \underline{u} + \frac{\nabla \rho \times \nabla p}{\rho^2} + \nabla \times \underline{f} + \nu \nabla^2 \underline{\omega}$$

advection of $\underline{\omega}$
baroclinic generation of $\underline{\omega}$
body force generation of $\underline{\omega}$
diffusion of $\underline{\omega}$

$(=0 \text{ if } \rho(p) \text{ (barotropic)})$
 $(=0 \text{ if } \underline{f} = -\nabla \pi)$

$\frac{D \underline{\omega}}{Dt}$

show: stretching & tilting of vortex lines

Non-dimensional form (barotropic & cons. body force)

$$\Rightarrow \frac{D \omega_i}{Dt} = \omega_j \frac{\partial u_i}{\partial x_j} + \frac{1}{Re} \frac{\partial \omega_i}{\partial x_j \partial x_j}$$

compare with eq. for material line element

$$\frac{D dl_i}{Dt} = \frac{\partial u_i}{\partial x_j} dl_j$$

For $Re \rightarrow \infty$ $\frac{D \omega_i}{Dt} = \frac{\partial u_i}{\partial x_j} \omega_j$



Helmholtz theorem for $Re \rightarrow \infty$:

- vortex lines are material lines

- i) stretching of vortex line produce ω_i like stretching of dl_i produce length
- ii) tilting of vortex line produce ω_i in one direction at expense of ω_i in another direction

Study terms in the vorticity equation.

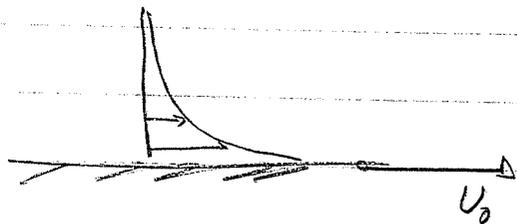
$$2D: \frac{\partial \omega_3}{\partial t} + u_1 \frac{\partial \omega_3}{\partial x_1} + u_2 \frac{\partial \omega_3}{\partial x_2} = \nu \nabla^2 \omega_3$$

no tilting & stretching in 2D

ex. Diffusion of vorticity: Stoke's problem

$$\omega_3 = \omega_2 = \omega(y, t)$$

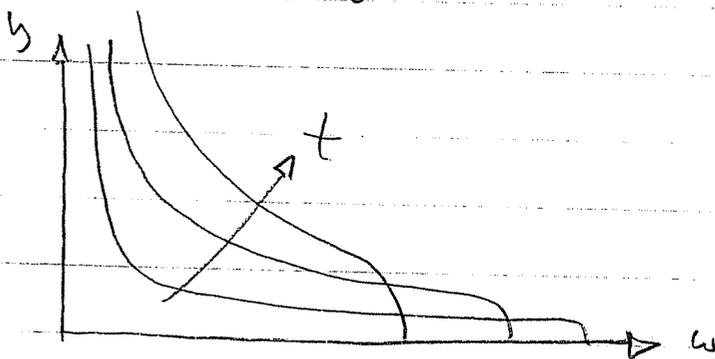
$$\frac{\partial \omega}{\partial t} = \nu \frac{\partial^2 \omega}{\partial y^2}$$



$$\omega = \frac{U_0}{\sqrt{\pi \nu t}} e^{-y^2/4\nu t}$$

$$\left(\omega_2 = \frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} = -\frac{\partial u}{\partial y} \right)$$

diffusion length scale $\delta(t) = \sqrt{4\nu t}$



vorticity is generated at the wall and diffuses into fluid above (but $-\nu \frac{\partial \omega}{\partial y} \Big|_{y=0} = 0; t > 0$)

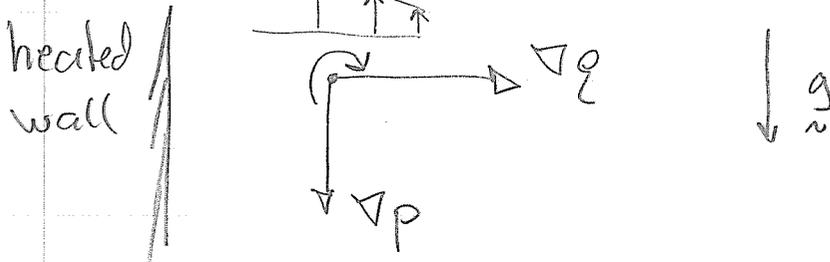
$$\text{note: } \int_0^{\infty} \omega dy = \int_0^{\infty} -\frac{\partial u}{\partial y} dy = U_0 = \text{constant}$$

ω concentrated at the wall for $t = 0^+$

Generation of vorticity.

- if flow is viscous and $\omega(t=0) = 0$, then vorticity is generated at solid boundaries and diffuses into flow.
- if f is non-conservative, then vorticity is generated by $\nabla \times f$
- if flow is not barotropic, $\rho(P, T)$, then vorticity is generated by

$$\frac{\nabla \rho \times \nabla p}{\rho^2}$$



$Re \gg 1$

